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# COMPARATIVE REACTIVITY OF SOME CALCAREOUS ROCKS AS SORBENTS TOWARDS SULPHUR DIOXIDE

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Abstract. The thermogravimetric method was used for studying the SO<sub>2</sub> binding reactivity of Estonian limestones and dolomites from different deposits. Chemical, X-ray, BET, a.o. methods were used for the characterization of the initial samples and the products of SO<sub>2</sub> binding. The experimental data were processed mathematically to determine the models of the SO<sub>2</sub> binding mechanism for all sorbents used. The results of this study confirmed the high reactivity of Estonian limestones and dolomites towards SO<sub>2</sub> — in some cases it is comparable to the reactivity of the reactive grade of CaCO<sub>3</sub>. The correlation between the reactivity of the samples and their specific surface area was observed.

Key words: limestone, dolomite, sulphur dioxide, sorption.

# INTRODUCTION

The extensive use of sulphur-containing fuels induces the acidic pollution of the atmosphere with sulphur dioxide, which requires a supplementary cleaning of flue gases. It is a serious problem for Estonia where the Estonian and the Baltic Thermal Power Plants operate on Estonian oil shale which contains about 1.5% of sulphur [<sup>1</sup>]. For the removal of acidic compounds from flue gases, the most

For the removal of acidic compounds from flue gases, the most common sorbents used are lime-containing materials: natural limestones, and dolomites and their derivatives, and industrial materials ashes containing free calcium-magnesium oxides  $[^{2-5}]$ . The explored resources of Estonian limestones and dolomites are estimated to be 200— 250 million m<sup>3</sup>, but their use in technology is confined to the cement and glass industries and the production of lime  $[^{6-8}]$ .

Our investigations were aimed at the comparative characterization of the reactivity of Estonian limestones and dolomites towards  $SO_2$  binding from the gaseous phase by a dry method. We used the thermogravimetric (TG) method [9-16]. Earlier, the high temperature oil-shale ashes have been used for the same purpose [17].

### **EXPERIMENTAL**

Estonian limestones and dolomites of different deposits (Adavere, Anelema, Karinu, Vasalemma, Väo, Kaarma, Maardu and shivers waste of Maardu limestone) with different  $CaCO_3$  and  $MgCO_3$  content were studied. For comparison, oil-shale furnace ash formed in the fluidized bed boiler (the so-called low-temperature ash), a limestone sample from Poland and calcium carbonate of reactive grade were used.

TG studies were carried out in isothermal conditions in the derivatograph OD-103 (MOM, Hungary), the calcination taking place in the atmosphere of air, the sulphation in the mixture of SO<sub>2</sub> and air, with the heating rate 10 K per min. The calcination was performed up to 900 °C in order to achieve a constant weight of the sample. When necessary, the sample was cooled down to the required temperature, after which the air enriched with SO<sub>2</sub> was led to the reaction chamber. Plate type Pt-crucibles were used. The thickness of the sample layer was 0.2–0.3 mm, the weight of the sample — 100 mg, the rate of the gas flow was 270 ml/min, and the partial pressure of SO<sub>2</sub> in the air—SO<sub>2</sub> mixture was 120 mm Hg.

The chemical composition and physical properties of the samples and their changes during the contact between the solid and gaseous phases were determined by using different methods of analysis — chemical, stereological (Videolab 2), X-ray (Dron 3M), BET-nitrogen dynamic desorption (sorptometer EMS-53), and others. The results for the initial samples are presented in Table 1.

As seen from Table 1, the sum of the contents of CaO and MgO varied from 51 to 59%. except for Maardu waste where it was 39.7%. The content of SiO<sub>2</sub> varied from 1 to 12%, the content of SO<sup>2-</sup><sub>4</sub> between 0-1%, and that of CO<sub>2</sub> from 39.4 to 43.3% (for Maardu waste - 34.8%). The content of CaO + MgO in the oil-shale ash was 73.1%, that of free CaO was 45.1%. The density of the samples was nearly the same: it varied from 2.88 to 2.99 g/cm<sup>3</sup>. The specific surface area (SSA) for Estonian limestones and dolomites ranged from 2.3 to  $5.7 \text{ m}^2/\text{g}$ , for Polish limestone it was 0.85 m<sup>2</sup>/g, and for oil-shale ash 1.6 m<sup>2</sup>/g. Two different fractions of the samples were used: the fine fraction and the coarse fraction. The mean particle size for the samples of the fine fraction ranged from 10.5 to 28 µm, for the samples of the coarse fraction it varied between 44 and 48 µm.

Two parameters were used to characterize the extent of interaction: the  $SO_2$  binding rate (mg  $SO_2$ /mg sample per min) and the  $SO_2$  binding capacity (mg  $SO_2$ /100 mg sample). The results of the TG investigations were used to determine the reaction mechanisms.

### **RESULTS AND DISCUSSION**

The characteristic TG-curve of limestone decomposition in the dynamic heating conditions, in air, with the following sulphation of the decomposed product in isothermal conditions, in an air-SO<sub>2</sub> mixture, is presented in Fig. 1. The results obtained in the temperature interval from 400 to 900 °C confirmed that the capacity to bind SO2 increased for all the materials studied when the temperature was increased, and it was considerable at 700 °C and above. During the first period of interaction, the  $SO_2$  binding rate was the more intensive the higher the temperature. For example, at 500 °C, the amount of the  $SO_2$  bound by the limestone of the Karinu deposit during the first 2 min was 8.8 mg per 100 mg of sample (62%) of the total amount of bound sulphur dioxide), the amount bound during the following 8 min was 5.4 mg. At 700 and 900 °C, the amount of the bound SO<sub>2</sub> after 2 min of contact with Karinu limestone was 72.9 mg and 98.6 mg SO<sub>2</sub> per 100 mg of sample, respectively, or 80 and 90%, as related to the total amount of the bound SO2 after 10 min of contact (Fig. 1).

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Parameters	Ada- vere D*	Karinu C**	Maardu C	Ane- lema D	Vão C	Vasa- lemma C	Kaarma D	Maardu waste C	Oil- shale ash	Polish C
Content wt %. of:	ti diia diia	nen nen kali	nn. riei	191		sul sul aQ	of and (al)	100	alci alci O <sub>2</sub>	ig G red restr e u
CaO Mg0	37.1	57.4 1.7	49.3 2.3	38.5 20.2	51.1 4.8	50.8 2.3	29.5 21.9	34.6 5.1	66.2 6.9	55.0 0.2
CaO free		1	1	1					45.1	In al
50°	≈0	0≈	1.1.	≈0	0.0	0.7	0.3	0.7	5.8	∞
SiO <sub>2</sub>	1.7	1.1	4.4	2.2	9.5	5.0	5.8	11.8	7.7	0.5
Fe2O3 A12O3	0.3	0.2	0.8	0.8	0.8	0.8	0.0	1.2	2.4	0.4
K <sub>2</sub> 0 CO <sub>2</sub>	43.3	0.1 41.5	0.1 39.4	0.2 43.3	0.1 40.8	0,1 41.1	43.0	34.8	0.9	43.4
MgCO3	37.2	3.6	4.8	42.5	10.2	4.8	46.0	10.7		0.4
Density. g/cm <sup>3</sup>	2.96	2.97	2.99	2.93	2.97	2.96	2.92	2.88	2.90	30.4
Specific surface area, m <sup>2</sup> /g	5.1	3.5	2.7	5.7	4.6	3.5	2.3	5.1	1.6	0.9
Mean particle size, µm	10.5	19	26	11	. 18	26	24	25	28	biv ol
* Dolomite, ** Caleite.										

of the sample, m, 10



Fig. 1. Thermogravimetric curves of calcination (up to 900 °C) and sulphation of Karinu limestone at different temperatures.

The more detailed comparison of different samples was carried out at 700 °C. On the basis of the SO<sub>2</sub> binding activity data of the samples, for 30 s of interaction between the solid and gaseous phases, the limestones and dolomites were divided into three groups. The best results were obtained for the dolomites of Adavere and Anelema deposits: the reaction proceeded with a high SO<sub>2</sub> binding rate — 1.19 and 0.89 mg SO<sub>2</sub>/mg sample per min, respectively, which means that 59.6 and 44.4 mg SO<sub>2</sub> per 100 mg sample were bound (Fig. 2). The binding rate of SO<sub>2</sub> by Maardu waste and Karinu limestone was approximately the same as that by Anelema dolomite — 0.87 and 0.81 mg SO<sub>2</sub>/mg sample per min, and the SO<sub>2</sub> binding capacity was 43.4 and 40.4 mg SO<sub>2</sub> per 100 mg of sample, respectively (Figs. 2 and 3).



Fig. 2. SO<sub>2</sub> binding rate (a) and binding capacity (b) of different fractions of Adavere and Anelema dolomites and Karinu limestone at 700 °C.

The limestones of Vasalemma, Väo and Maardu deposits form the second group. For this group, the  $SO_2$  binding rate ranges from 0.35 to 0.41 mg/mg sample per min (the  $SO_2$  binding capacity ranges from 17.7 to 20.7 mg per 100 mg sample) (Fig. 3). The poorest results were obtained for Kaarma dolomite: the  $SO_2$  binding rate during 30 s was only 0.03 mg  $SO_2$ /mg sample per min (6.6 mg  $SO_2$  per 100 mg sample). When using oil-shale ash, the  $SO_2$  binding rate was 0.36 mg  $SO_2$ /mg sample per min, and the  $SO_2$  binding capacity was 17.8 mg  $SO_2$  per 100 mg sample (Fig. 3).



Fig. 3. SO<sub>2</sub> binding rate (a) and binding capacity (b) of the fine fraction of different samples at 700 °C.

When the contact time was extended up to 2 min, the amount of the bound SO<sub>2</sub> increased for Adavere and Anelema dolomites and Karinu limestone 1.5–2 times, i. e. up to 73–89 mg SO<sub>2</sub> per 100 mg sample. This means that the SO<sub>2</sub> binding rate during the 2 min of contact was between 0.37 and 0.45 mg SO<sub>2</sub>/mg sample per min. For the second group of limestones (including Maardu waste), the binding capacity of SO<sub>2</sub> increased 1.5–4 times, but the total amount of the bound SO<sub>2</sub> was smaller than for the first group — from 61 to 67 mg SO<sub>2</sub> per 100 mg sample. The high reactivity of Maardu waste in the first seconds of interaction can be explained, in addition to the high SSA, by the relatively high content of Fe<sub>2</sub>O<sub>3</sub> — 1.8%. Ferric oxide is a well-known promotor for oxidizing SO<sub>2</sub>, and the reaction CaO+SO<sub>3</sub> → CaSO<sub>4</sub> [<sup>15, 18</sup>].

The third group, the Kaarma dolomite bound during the following 90 s of contact 14 times more  $SO_2$  than during the first 30 s, but the total amount of the bound  $SO_2$  was again smaller than for the other limestone and dolomite samples. The sample of oil-shale ash bound, during 2 min of contact, 46.5 mg  $SO_2$  per 100 mg sample with the rate of 0.23 mg  $SO_2/mg$  sample per min.

Comparing the  $SO_2$  binding capacity data after 2 and 10 min of contact (Figs. 2 and 3), it was concluded that during the first 2 min, as a rule,

70-85% of the total amount of captured by sorbents sulphur dioxide was bound, with the exception of Maardu waste which bound up to 91% and Kaarma dolomite which bound only 59%. Oil-shale ash bound 68.5% of the total amount of the bound SO<sub>2</sub> in the first 2 min.

The X-ray data confirmed that, at 500 °C, when using samples of limestone, a part of  $SO_2$  was bound with the formation of  $CaSO_3$ , and the other part was bound as CaSO<sub>4</sub>. As a result of oxidation and decomposition of calcium sulphite at 600-700 °C, according to the following equations [9, 13, 14, 16]: CaSO<sub>3</sub>+1/2O<sub>2</sub>  $\rightarrow$  CaSO<sub>4</sub> and 4CaSO<sub>3</sub>  $\rightarrow$  CaS+  $+3CaSO_4$ , CaS and traces of CaSO<sub>3</sub> were identified, besides CaSO<sub>4</sub> as the main product of sulphation. At 900 °C, the main S-containing product was  $CaSO_4$ , the by-product was CaS. The presence of CaO might be explained also by its secondary formation during the reaction  $[^{16}]$ :  $3CaSO_4 + CaS \longrightarrow 4CaO + 4SO_2$ . Platinum as the crucible material can influence, as a promotor, the sulphation process of lime  $\begin{bmatrix} 16 \end{bmatrix}$ . In the products of sulphation of dolomite at 500 °C, CaSO<sub>3</sub>, CaSO<sub>4</sub> and MgSO<sub>3</sub> were identified, at 700 °C - CaSO<sub>4</sub>, MgSO<sub>4</sub> and traces of MgSO<sub>3</sub>. At 900 °C, the main products of sulphation were CaSO<sub>4</sub> and MgSO<sub>4</sub>. A certain amount of CaS, CaO and traces of MgO were also identified. These results confirmed that, in our experimental conditions, MgO took part in the binding of SO<sub>2</sub> not only below 800 °C [<sup>12</sup>].



Fig. 4. Dependence of  $SO_2$  binding rate on the specific surface area of the sorbent.





The SSA is one of the parameters which characterizes well the natural limestones-dolomites as sorbents for the removal of  $SO_2$  from flue gases [19, 20]. There exists a correlation between the reactivity of samples towards  $SO_2$  binding and the SSA of the initial samples (Fig. 4). Only two of the samples have a comparatively low SO<sub>2</sub> binding rate, as might be expected on the basis of the SSA data. These are Vao limestone and Maardu waste which both contain twice as much insoluble residue (SiO<sub>2</sub>) as the others and, apart from that, Maardu waste contains Ca, Mg-oxides about 10% less than the other samples. The changes in the SSA data after 10 min of processing of the samples in the atmosphere of  $air-SO_2$  mixture are shown, for different temperatures, in Fig. 5. The SSA value decreases rapidly during the binding of SO<sub>2</sub>, and the higher the SSA data for the initial sample, the bigger the difference between the initial sample and the product. The SSA value for oil-shale ash did not actually change during the interaction between SO<sub>2</sub> and the sorbent. The stereological analysis of the samples confirmed that during calcination and sulphation the mean particle size of Estonian limestones and dolomites increased by 6 - 12%.

A series of experiments for studying the influence of the particle size on desulphurization of the gaseous phase was carried out by using the samples of Adavere and Anelema dolomite and Karinu limestone with a mean particle size from 44 to 48  $\mu$ m (coarse fraction). In that case the SO<sub>2</sub> binding rate during the first 30 s of contact was 0.67 for Anelema dolomite, 0.39 for Adavere dolomite and 0.37 mg SO<sub>2</sub>/mg sample per min for Karinu limestone. During 2 min of contact the amount of the sulphur dioxide bound by Anelema dolomite increased up to 72.5 mg (or 85% of the total amount of the sulphur dioxide bound during 10 min), and the amount bound by Adavere dolomite and Karinu limestone increased up to 54.0 mg (73%) and 58 mg (78%) per 100 mg sample, respectively (Fig. 2). Comparing the results obtained for fine and coarse fractions of limestones or dolomites, it may be concluded that the increase in the mean particle size by 2.5—3.5 times corresponds to the decrease in the binding capacity of SO<sub>2</sub> from 20 to 35%.



Fig. 6. SO<sub>2</sub> binding rate (a) and binding capacity (b) of different samples at 900 °C.

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The experiments for comparing the  $SO_2$  binding efficiency of Estonian limestones and dolomites with Polish limestone were carried out at 900 °C. The results confirmed that the  $SO_2$  binding rate during the first minutes of contact was 2—3 times higher for Adavere dolomite and Karinu limestone and twice lower for Vasalemma limestone than for Polish limestone. The amount of  $SO_2$  bound by these Estonian limestones during 10 min of contact exceeded by 5—10% the amount bound by the Polish limestone (Fig. 6).

The comparison of the  $SO_2$  binding capacity of the first group of limestones and dolomites with that of reactive grade  $CaCO_3$  was carried out in dynamic heating conditions at the rate 5 °C/min, up to 1000 °C. The samples of Adavere and Anelema dolomite had approximately the same  $SO_2$  binding capacity as the reactive calcium carbonate — only 2.7 and 8.5% less, respectively. Karinu limestone and Maardu waste bound 15.9 and 25.4% of  $SO_2$  less, respectively, than  $CaCO_3$ .

### MATHEMATICAL PROCESSING OF THE EXPERIMENTAL DATA

The experimental data were processed mathematically to determine the possible reaction mechanisms for the tested samples. Nine well-known equations describing different reaction mechanisms  $g(\alpha)$  were used to calculate the rate constant  $K(1/\min)$  as a slope in:

 $g(\alpha) = K \cdot t$ ,

1.	$g(\alpha) = [-\ln(1-\alpha)]^{1/3}$	Avrami-Erofeejev, nuclei growth
2.	$g(\alpha) = [-\ln(1-\alpha)]^{1/2}$	Avrami-Erofeejev, nuclei growth
3.	$g(\alpha) = 1 - (1 - \alpha)^{1/2}$	Contracting cylinder
4.	$g(\alpha) = 1 - (1 - \alpha)^{1/3}$	Contracting sphere
5.	$g(\alpha) = -\ln(1-\alpha)$	Mampel, unimolecular law — first order kinetics
6.	$g(\alpha) = \alpha^2$	One-dimensional diffusion
7.	$g(\alpha) = \alpha + (1-\alpha) \cdot \ln(1-\alpha)$	Valensi, two-dimensional diffusion
8.	$g(\alpha) = 1 - 2/3\alpha - (1 - \alpha)^{2/3}$	Ginstling-Brounshtein, three-dimension- al diffusion
9.	$g(\alpha) = [1 - (1 - \alpha)^{1/3}]^2$	Jander, three-dimensional diffusion

and

t - time, min.

The last point of every TG-curve was taken as 100% of conversion, the calculations were made for the conversion range of  $\alpha = 0-75\%$  at 700 °C.

In each case we looked for the maximum value of the regression coefficient  $R^2$  to get the best fit but for some of these mechanisms all values of K are presented for the sake of a better comparison of different samples.

Eleven different samples were investigated and the results of the calculations are presented in Table 2. As Table 2 shows, all the samples can be divided into two groups according to the reaction mechanism. Fine fractions of Adavere, Anelema and Karinu samples belong to the group of the Jander three-dimensional diffusion model No. 9, the biggest Kvalue of this group corresponding to Adavere dolomite. All the other limestone and dolomite samples studied, as well as the oil-shale ash, belong to the first order kinetics model No. 5, the biggest K values

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(1)

corresponding to Maardu waste and Vasalemma limestone, the smallest one to Väo limestone. The highest  $SO_2$  binding rates were achieved by Maardu waste, Adavere dolomite and Vasalemma limestone, the lowest by Väo limestone.

Table 2

Sample	R <sup>2</sup>	<i>K</i> , 1/min	K, 1/min for models	
erade C100, was carried			No. 5	No. 9
Model No. 5				
Maardu, waste	0.9805	1.6038	1.6038	0.4434
Vasalemma, fine	0.9708	0.9677	0.9677	0.2651
Anelema, coarse	0.9877	0.9092	0.9092	0.2572
Karinu, coarse	0.9977	0.6644	0.6644	0.1835
Adavere, coarse	0.9992	0.5838	0.5838	0.1630
Maardu, fine	0.9889	0.5580	0.5580	0.1544
Oil-shale ash	0.9981	0.4874	0.4874	0.1377
Kaarma, fine	0.9688	0.4470	0.4470	0.1200
Väo, fine	0.9941	0.4024	0.4024	0.1146
Model No. 9			ecine stal o	
Adavere, fine	0.9519	0.2701	0.9588	0.2701
Anelema, fine	0.9831	0.2072	0.7302	0.2072
Karinu, fine	0.9409	0.1448	0.5000	0.1448

#### Kinetic constant for samples

### CONCLUSIONS

1. Considering the reactivity towards SO<sub>2</sub> binding, Estonian limestones and dolomites, investigated in this study, fall into three groups:

 Adavere and Anelema dolomites, Karinu limestone and shivers waste of crushed Maardu limestone;

- Vasalemma, Väo and Maardu limestones;

- Kaarma dolomite

The  $SO_2$  binding efficiency of Maardu waste decreased rapidly when the contact time was prolonged over 60 s.

The samples of Adavere and Anelema dolomite have approximately the same level of  $SO_2$  binding capacity as the reactive grade  $CaCO_3$ .

2. The low-temperature oil-shale ash has approximately the same level of reactivity towards  $SO_2$  as the limestones of the second group.

3. Up to 500-550 °C, a part of the bound SO<sub>2</sub> was identified as CaSO<sub>3</sub> and MgSO<sub>3</sub>; their oxidation as well as the decomposition of CaSO<sub>3</sub> took place at 600-700 °C. At 900 °C, the main product of sulphation was CaSO<sub>4</sub> when limestones were used, and CaSO<sub>4</sub> and MgSO<sub>4</sub> when dolomites were used.

4. The SSA of sorbents decreases rapidly during the sulphation; the increase in the mean particle size ranged from 6 to 12%. A correlation between the SSA of sorbents and their reactivity towards SO<sub>2</sub> was observed; the 2.5—3.5 times increase in the mean particle size corresponds to the decrease in the amount of the bound SO<sub>2</sub> from 20 to 35%.

5. Mathematical data processing confirmed that the reaction mechanism of  $SO_2$  binding by fine fractions of Adavere and Anelema dolomite and Karinu limestone corresponds to the Jander three-dimensional diffusion model. The reaction mechanism of the other studied sorbents corresponds to the first order kinetics model.

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# REFERENCES

- Ots, A. Formation of air-polluting compounds while burning oil shale. In: Energy and Environment 1991. Atlanta, 1991, 284—290.
- Szekely, J., Evans, J. W., Sohn, H. Y. Gas-Solid Reactions. Academic Press, New York etc., 1976.
- Hupa, M. Fluidized Bed Technology, Basics and Large Scale Applications, Emissions. Lecture at the Nordic-IFRF Course "Solid Fuels Utilization and Environment", 25th-27th Aug. 1992, Lohusalu, Estonia. Vol. 1, Lecture No. 8.
- Staudinger, G., Krammer, G., Eckerstorfer, K. 90% SO<sub>2</sub>-removal with dry limestone-ARA-process. — In: 1990 SO<sub>2</sub> Control Symposium. New Orleans, Louisiana, 1990.
- Mustonen, J., Sjöholm, P. Fläkt Drypac Flue Gas Desulphurization Plant at Salmisaari. — Fläkt Review, n. d., No. 73, 4—7.
- National Report of Estonia to UNCED 1992. United Nations Conf. on Environment and Development. Rio de Janeiro, Brazil, 3-14 June 1992. Ministry of the Environment, Republic of Estonia. Tallinn, 1992.
- 7. Raudsep, R., Räägel, V., Savitskaja, L., Orru, M., Kattai, V. Eesti maapõuerikkusi. RE Eesti Geoloogiakeskus, Tallinn, 1993.
- Тээдумяэ А. Минерально-сырьевые ресурсы Эстонской ССР для промышленности строительных материалов. Валгус, Таллини, 1988.
- 9. Ingraham, T. R., Marier, P. Mechanism of the absorption of SO<sub>2</sub> by limestone. JAPCA, 1971, 21, 6, 347.
- Spitsbergen, U., Vincent, C. J., Longe, T. A. Comparison of selected European limestones for desulphurization of gases from atmospheric fluidized bed combustion. — J. Inst. Energy, 1981, June, 94—99.
- Hakvoort, G., Van den Bleek, C. M., Schouten, J. C., Valkenburg, P. J. M. TG study of sorbent materials for desulfurization of combustion gases at high temperature. — Thermochim. Acta, 1987, 114, 103—108.
- 12. Wiedeman, H.-G., Boller, A., Bayer, G. Thermogravimetric studies of the reactions between dolomite and sulfur dioxide. Solid State Ionics, 1990, **43**, 53—60.
- Wieczorek-Ciurowa, K. Catalytic sulphation of limestone/lime with platinum. J. Thermal. Anal., 1992, 38, 2101—2107.
- Marsh, D. W., Ulrichson, D. L. Rate and diffusional study of the reaction of calcium oxide with sulfur dioxide. — Chem. Eng. Sci., 1985, 40, 3, 423—433.
- Marier, P., Dibbs, H. P. The catalytic conversion of SO<sub>2</sub> to SO<sub>3</sub> by fly ash and the capture of SO<sub>2</sub> and SO<sub>3</sub> by CaO and MgO. — Thermochim. Acta, 1974, 78, 155—165.
- Wieczorek-Ciurowa, K. The thermal behaviour of compounds in the Ca—S—O system. — J. Thermal. Anal., 1992, 38, 523—530.
- Kaljuvee, T., Kuusik, R. Desulphurization of flue gases by oil shale ash. Oil Shale, 1993, 10, 33-43.
- Yang, R. T., Shen, M.-S., Steinberg, M. Fluidized-bed combustion of coal with lime additives: Catalytic sulfation of lime with iron compounds and coal ash. — Environ. Sci. Technol., 1978, 12, 8, 915—918.
- Gullett, B. K., Blom, J. A., Cunningham, R. T. Porosity, surface area and particle size effects of CaO reacting with SO<sub>2</sub> at 1100 °C. — Reactivity of Solids, 1988, 6, 263-275.
- Cole, J. A., Kramlich, J. C., Seeker, W. R., Heap, M. P., Samuelsen, G. S. Activation and reactivity of calcareous sorbents towards sulfur dioxide. — Environ. Sci. Technol., 1985, 19, 11, 1065—1072.

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### MÕNINGATE LUBJAKIVIMITE VÄÄVELDIOKSIIDI SIDUMISVÕIME KÕRVUTAV UURIMINE

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Kasutades termogravimeetria meetodit uuriti mõningate Eesti lubjakivide ja dolomiitide võimet siduda SO<sub>2</sub>. Lähteproovide ja SO<sub>2</sub>-sidumisproduktide iseloomustamiseks kasutati keemilist, röntgendifraktsioon-, BET eripinna määramise ja teisi meetodeid. Katsetulemusi matemaatiliselt töödeldes määrati kõikide uuritud sorbentide SO<sub>2</sub> sidumismehhanismi mudelid. Saadud tulemused kinnitavad Eesti lubjakivide ja dolomiitide kõrget aktiivsust vääveldioksiidi sidumisel. Mõningate proovide puhul on see võrreldav reaktiivse CaCO<sub>3</sub> sidumisaktiivsusega. Täheldati head korrelatsiooni uuritud proovide SO<sub>2</sub> sidumisaktiivsuse ja eripinna vahel.

# СРАВНИТЕЛЬНОЕ ИССЛЕДОВАНИЕ АКТИВНОСТИ СВЯЗЫВАНИЯ ДИОКСИДА СЕРЫ НЕКОТОРЫМИ ИЗВЕСТКОВЫМИ РУДАМИ

### Тийт КАЛЬЮВЕЕ, Андрес ТРИККЕЛ, Рейн КУУСИК

Термогравиметрическим методом анализа изучена активность связывания диоксида серы некоторыми эстонскими природными известковыми рудами. Для характеристики исходных образцов и продуктов связывания SO<sub>2</sub> использованы химический, рентгенофазовый, БЭТ-десорбционный и др. методы анализа. По результатам экспериментов определены модели механизма связывания SO<sub>2</sub> для всех изученных сорбентов. Установлено, что активность некоторых эстонских известковых руд при связывании SO<sub>2</sub> сравнима с активностью реактивного CaCO<sub>3</sub>. Существует хорошая корреляция между активностью связывания SO<sub>2</sub> и удельной поверхностью образцов.